

学号

姓名

1. 1st Law

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2.  $\oint W_{rev} \equiv ?$

3.  $H \equiv ?$

4. Heat capacity.  $C \equiv ?$

$$- \Delta P$$

$$- \delta P$$

$$= \frac{Q_{rev}}{T} \leftarrow$$

$$v = \frac{-Q_{rev}}{T}$$

$$- \frac{Q_{irr}}{T}$$

$$\left( \frac{Q_{irr}}{T} + \frac{Q_{def}}{T} \right) = \frac{Q_{rev}}{T}$$

$$Q_{irr} \quad \Delta S_{tot} > 0$$

$$\Delta S_{production} = \frac{Q_{def}}{T}$$

$$\left[ \begin{array}{l} \text{Irrev. } \Delta S_{pro} > 0 \\ \text{Rev. } \Delta S_{pro} = 0 \end{array} \right.$$

Condensation Only:

$$\left[ \begin{array}{l} \text{Irr. } -P_{ext} + \Delta P \\ \text{rev. } (P_{ext} + \delta P) \approx P_{ext} \end{array} \right.$$

Assume: one mole H<sub>2</sub>O condensed:  $\downarrow V$

work done on cylinder

$$W_{irr} = (P_{ext} + \delta P) \cdot V$$

$$W_{rev} = P_{ext} \cdot V = W_{irr}$$

cylinder:

$$\text{rev. } \Delta U = -Q_{rev} + W_{min}^{rev.}$$

$$\text{Irr. } \Delta U = -Q_{irr} + W_{irr.}$$

$\Delta S_{\text{production}} = \frac{Q_{\text{deg}}}{T}$   
 Irrev.  $\Delta S_{\text{pro}} > 0$   
 Rev.  $\Delta S_{\text{pro}} = 0$

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Condensation Only:  
 Irr.  $P_{\text{ext}} + \Delta P$   
 Rev.  $(P_{\text{ext}} + \delta p) \approx P_{\text{ext}}$   
 Assume: one mole H<sub>2</sub>O condensed:  $\downarrow$   
 Work done on cylinder  
 $W_{\text{irr}} = (P_{\text{ext}} + \delta p) \cdot V$   
 $W_{\text{rev}} = P_{\text{ext}} \cdot V = W_{\text{min}}$

cylinder:  
 Rev.  $\Delta U = -Q_{\text{rev}} + W_{\text{min}}^{\text{rev}}$   
 Irr.  $\Delta U = -Q_{\text{irr}} + W_{\text{irr}}$   
 $\therefore (W_{\text{irr}} - W_{\text{min}}) = Q_{\text{irr}} - Q_{\text{rev}}$   
 $> 0 = \left[ - (Q_{\text{rev}} - Q_{\text{irr}}) \right] > 0$   
 $\quad \quad \quad \parallel$   
 $\quad \quad \quad Q_{\text{deg}}$

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Rev.  $\left[ \begin{array}{l} \Delta S_{\text{resv}} = \frac{Q_{\text{rev}}}{T} \\ \Delta S_{\text{cyl}} = -\frac{Q_{\text{rev}}}{T} \end{array} \right] \Delta S_{\text{tot}} = 0$

Irr.  $\left[ \begin{array}{l} \Delta S_{\text{resv}} \\ \Delta S_{\text{cyl}} \end{array} \right]$

$\Delta S_{\text{production}} = \frac{Q_{\text{deg}}}{T}$   
 Irrev.  $\Delta S_{\text{pro}} > 0$   
 Rev.  $\Delta S_{\text{pro}} = 0$

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Condensation Only:  
 $P_{\text{ext}} + \Delta P$   
 $(P_{\text{ext}} + \delta p) \approx P_{\text{ext}}$   
 Assume: one mole H<sub>2</sub>O condensed:  $\downarrow$   
 Work done on cylinder  
 $W_{\text{irr}} = (P_{\text{ext}} + \delta p) \cdot V$   
 $W_{\text{rev}} = P_{\text{ext}} \cdot V = W_{\text{min}}$

cylinder:  
 Rev.  $\Delta U = -Q_{\text{rev}} + W_{\text{min}}^{\text{rev}}$   
 Irr.  $\Delta U = -Q_{\text{irr}} + W_{\text{irr}}$   
 $\therefore (W_{\text{irr}} - W_{\text{min}}) = Q_{\text{irr}} - Q_{\text{rev}}$   
 $> 0 = \left[ - (Q_{\text{rev}} - Q_{\text{irr}}) \right] > 0$   
 $\quad \quad \quad \parallel$   
 $\quad \quad \quad Q_{\text{deg}}$

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Rev.  $\left[ \begin{array}{l} \Delta S_{\text{resv}} = \frac{Q_{\text{rev}}}{T} \\ \Delta S_{\text{cyl}} = -\frac{Q_{\text{rev}}}{T} \end{array} \right] \Delta S_{\text{tot}} = 0$

Irr.  $\left[ \begin{array}{l} \Delta S_{\text{resv}} \\ \Delta S_{\text{cyl}} \end{array} \right]$   
 Hint \*

$-Q_{rev} + W_{min}^{rev}$   
 $-Q_{irr} + W_{irr}$   
 $min \Rightarrow Q_{irr} - Q_{rev}$   
 $= [-(Q_{rev} - Q_{irr})] > 0$   
 $\parallel$   
 $Q_{deg}$   
 $Q_{rev} = \frac{Q_{deg}}{T} \quad \Delta S_{tot} = 0$   
 $l. = -\frac{Q_{rev}}{T}$

$I_{irr} \left[ \begin{aligned} \Delta S_{rev} &= \frac{Q_{irr}}{T} \\ \Delta S_{cyl} &= \left(\frac{Q_{irr}}{T}\right) \left[\frac{Q_{deg}}{T}\right] = \frac{-Q_{rev}}{T} \end{aligned} \right.$   
 $\Delta S_{tot} = \frac{Q_{deg}}{T} > 0$   
 $cyl: \Delta S_{rev} = \Delta S_{irr}$   
 $\Delta S_{prod} = \frac{Q_{deg}}{T} > 0$   
 $S: \text{definition?}$   
 $Hint * S: \text{state function!}$

$2. = \left(\frac{Q_{irr}}{T}\right) \left[\frac{Q_{deg}}{T}\right] = \frac{-Q_{rev}}{T}$   
 $\frac{Q_{deg}}{T} > 0$   
 $v = \Delta S_{irr}$   
 $\frac{Q_{deg}}{T} > 0$   
 $\text{tion?}$   
 $\text{function!}$

**Summary:**  
 1. Universe:  
 $I_{rev}: \begin{cases} \Delta S_{tot} > 0 \\ \Delta S_{prod} > 0 \end{cases}$   
 2. Rev.:  
 $\begin{cases} \Delta S_{tot} = 0 \\ \Delta S_{prod} = 0 \end{cases}$   
 3. cylinder:  
 $\Delta S_{rev} = \Delta S_{irr}$   
 $\Rightarrow S: \text{state function}$

# Carnot Cycle (Engine)

Inverse:  
 $\Delta S_{\text{rev}} > 0$   
 $\Delta S_{\text{prod}} > 0$   
 $\Delta S_{\text{rev}} = 0$   
 $\Delta S_{\text{prod}} = 0$   
 cylinder:  
 $\Delta S_{\text{rev}} = \Delta S_{\text{irrev}}$   
 $S$ : state function

## (Rev. + Isothermal) Compression

one mole ideal gas

$$(V_A, T) \xrightarrow{\text{state A}} (V_B, T) \quad (V_B < V_A) \quad \text{state B}$$

$$\therefore dT = 0 \quad \therefore \Delta U = 0 \quad \Delta Q = \Delta W$$

$$\Delta W = \int_{V_A}^{V_B} P \cdot dV = RT \ln\left(\frac{V_B}{V_A}\right) = \Delta Q$$

$$\Delta S_{\text{gas}} = \frac{Q_{\text{rev}}}{T} = \frac{W_{\text{rev}}}{T} = R \cdot \ln\left(\frac{V_B}{V_A}\right)$$

$$\Delta S_{\text{reser.}} = -\frac{Q_{\text{rev}}}{T} = -\Delta S_{\text{gas}}$$

(Engine)  
 (Rev + Adiabatic) Process  
 gas

$$(V_B, T) \quad (V_B < V_A) \quad \text{state B}$$

$$\Delta Q = \Delta W$$

$$\left(\frac{V_B}{V_A}\right) = \Delta Q$$

$$R \cdot \ln\left(\frac{V_B}{V_A}\right)$$

$S_{\text{gas}}$

## (Rev + Adiabatic) Process

Expansion

$$\text{state A} \xrightarrow{\text{Rev}} \text{state B}$$

$$(P_A, T_A) \longrightarrow (P_B, T_B)$$

$$P_A > P_B$$

$$\text{Adia. } \Delta Q = 0 \quad \text{Ideal gas: } PV^\gamma = \text{const}$$

$$\downarrow$$

$$\Delta S = 0 \Leftrightarrow \text{constant entropy (Isentropic) (Rev + Adia.)}$$

$$(P_A, T_A) \xrightarrow{\text{Ir.}} (P_B, T_B')$$

$$\therefore Q_{\text{rev}} > 0 \quad \therefore T_B' > T_B$$

Process

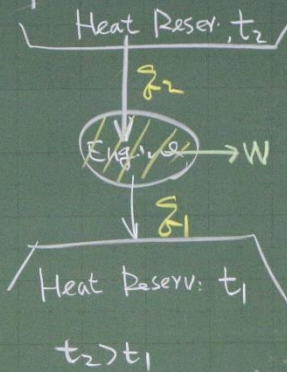
to B  
( $T_B$ )

ideal gas:  $PV = \text{const}$

constant entropy  
(Isentropic)  
(Rev + Adia.)

( $T'_B$ )  
 $\therefore T'_B > T_B$

### § Properties of Heat Engine



Efficiency:  $\eta \equiv \frac{W}{Q_2}$

- 2. (Isothermal + Rev)
- 2. (Adia. + Rev.)

"distance"

$W = (W_1 + W_2 + W_3 + W_4)$   
= area.

cycle:  $\Delta U = 0$   
 $\therefore \Delta W = \Delta Q = Q_2 - Q_1$   
 $\therefore \eta_{\text{Carnot}} = \left(\frac{\Delta W}{Q_2}\right) = \left(\frac{Q_2 - Q_1}{Q_2}\right)$

Carnot Engine.

Max. efficiency !!

cylinder:

Rev:  $\Delta U = -Q$

Irr:  $\Delta U = -Q$

$\therefore (W_{\text{irr.}} - W_{\text{rev.}})$

$\therefore > 0$


Rev:  $\int \Delta S_{\text{rev}}$   
 $\Delta S_{\text{cyl.}} =$

2: (Isothermal + Rev)

2: (Adia. + Rev.)

"ce"

$$W = (W_1 + W_2 + W_3 + W_4)$$

= area. 

cycle:  $\Delta U = 0$

$$\therefore \Delta W = \Delta Q = \int_2^1 p_2 - p_1$$

$$\eta_{\text{Carnot}} = \left( \frac{\Delta W}{Q_2} \right) = \left( \frac{p_2 - p_1}{p_2} \right)$$

### Carnot Engine.

Max. efficiency !!

$t_1, t_2$  Temp ?

proof ?

$$\frac{Q}{T}$$

cylinder:

$$\text{Rev: } \Delta U = -Q_{\text{rev}}$$

$$\text{Irr: } \Delta U = -Q_{\text{irr}}$$

$$\therefore (W_{\text{irr}} - W_{\text{rev}}) = Q_{\text{irr}}$$

$$\therefore > 0 = -(\dots)$$

$$\text{Rev: } \Delta S_{\text{rev}} = -$$

$$\Delta S_{\text{cyl}} = -\frac{Q}{T}$$